

# UNIVERSITI TEKNIKAL MALAYSIA MELAKA

# APPLICATION OF SIMULATED KALMAN FILTER ALGORITHM IN TUNING PID CONTROLLER'S PARAMETERS FOR COUPLED TANK SYSTEM

This report is submitted in accordance with the requirement of the Universiti Teknikal Malaysia Melaka (UTeM) for the Bachelor of Electrical Engineering Technology (Electronic Industries) with Honours.

By

# RABIATUL NURELISSA BINTI HASSAN B071510784 940403-03-5014

### FACULTY OF ELECTRICAL AND ELECTRONIC ENGINEERING

### TECHNOLOGY

2018



# UNIVERSITI TEKNIKAL MALAYSIA MELAKA

### BORANG PENGESAHAN STATUS LAPORAN PROJEK SARJANA MUDA

### TAJUK: APPLICATION OF SIMULATED KALMAN FILTER ALGORITHM IN **TUNING PID CONTROLLER'S PARAMETERS FOR COUPLE TANK SYSTEM**

SESI PENGAJIAN: 2018/19 Semester 2

### Saya : RABIATUL NURELISSA BINTI HASSAN

mengaku membenarkan Laporan PSM ini disimpan di Perpustakaan Universiti Teknikal Malaysia Melaka (UTeM) dengan syarat-syarat kegunaan seperti berikut:

- 1. Laporan PSM adalah hak milik Universiti Teknikal Malaysia Melaka dan penulis.
- 2. Perpustakaan Universiti Teknikal Malaysia Melaka dibenarkan membuat salinan untuk tujuan pengajian sahaja dengan izin penulis.
- 3. Perpustakaan dibenarkan membuat salinan laporan PSM ini sebagai bahan pertukaran antara institusi pengajian tinggi.
- 4. **\*\***Sila tandakan (X)

	SULIT	(Mengandungi maklumat yang berdarjah keselamatan atau kepentingan Malaysia sebagaimana yang termaktub dalam AKTA RAHSIA RASMI 1972)		
	TERHAD	(Mengandungi maklumat TERHAD yang telah ditentukan oleh organisasi/badan di mana penyelidikan dijalankan)		
X	TIDAK TERHA	D		
		Disahkan oleh:		
Alamat Teta	1	T HASSAN AMAR FAIZ BIN ZAINAL ABIDIN Cop Rasmi Penyelia:		
	Kampung Kelar			
17040 Pasir	Mas			
Kelantan.				
Tarikh:		Tarikh:		
		u TERHAD, sila lampirkan surat daripada pihak berkuasa/organisasi kali sebab dan tempoh laporan PSM ini perlu dikelaskan sebagai SULIT		

### DECLARATION

I hereby, declared this report entitled "APPLICATION OF SIMULATED KALMAN FILTER ALGORITHM IN TUNING PID CONTROLLER PARAMETERS FOR COUPLE TANK SYSTEM" is the results of my own research except as cited in references.

Signature	:	
Author's Name	:	RABIATUL NURELISSA BINTI HASSAN
Date	:	

### APPROVAL

This report is submitted to the Faculty of Engineering Technology of UTeM as a partial fulfillment of the requirements for the degree of Bachelor of Electrical Engineering Technology (Electronics Industrial) with Honours. The member of the supervisory is as follow:

Signature:	
Supervisor :	AMAR FAIZ BIN ZAINAL ABIDIN

#### ABSTRAK

Dalam dunia hari ini, aplikasi sistem tangki pasangan, menjadi bahagian yang tidak dapat dielakkan khusus dalam industri proses kimia di mana ia memenuhi permintaan teknologi proses yang semakin berkembang. Minat dunia dalam teknologi industri proses terus berkembang apabila sistem tangki pasangan menjadi popular dalam masalah penanda aras klasik kerana ciri tingkah laku fasa bukan linear dan tidak minimum. Selain itu, proses aliran dan paras cecair di dalam tangki menjadi isu utama di mana sistem memerlukan cecair untuk dipam, disimpan di dalam tangki dan kemudian didorong ke tangki lain secara automatik. Oleh itu, cadangan projek ini dengan parameter PID optimum untuk mengawal tahap 10cm paras air yang diingini dan tindak balas sementara keadaan tetap sistem tangki yang digabungkan menggunakan pengoptimuman Penapis Simulasi Kalman. Analisa hubungan antara bilangan agen Kalman berbanding bilangan lelaran yang dilakukan. Hasil yang diperoleh adalah dibandingkan dengan bacaan sebelumnya. Penemuan menunjukkan bahawa Penapis Simulasi Kalman melakukan lebih baik dalam sistem tangki yang digabungkan berbanding dengan Penguasan zarah Kecergasan Partikel Swarm dan Prioriti berdasarkan Prioriti.

v

#### ABSTRACT

In today's world, the application of couple tank system, become an inescapable part specifically in chemical process industries where it was met out the expanding process technologies requests. The world interest in process industry technologies is continually expanding when the couple tank system becomes popular in classical benchmark control problem due to the behavior of the non-linear and non-minimum phase characteristic. Furthermore, the flow process and liquid level in the tanks become the main issue where the system required the liquid to be pumped, kept in the tank and then driven to another tank automatically. Hence, the proposed of this project by optimal PID parameters in order to controlling the 10cm of the desired water level and steady state, transient response of coupled tank system using the Simulated Kalman Filter optimization. Analysis on the relationship between the number of Kalman agents versus number of iterations is done. The result obtained was benchmarked with previous literature. The findings show that Simulated Kalman Filter performs better in coupled tank system compared to Particle Swarm and Priority based Fitness Particle swarm optimization.

#### DEDICATION

To my adored parents, wholly the lecturers, exclusively my supervisor Amar Faiz Bin Zainal Abidin and the late Ir. Nik Azran Bin Abdul Hadi, all my friends and relatives. Thousands of appreciations and sincere thankfulness from the bottom of my heart for all the understanding and sacrifice throughout my entire duration in pursuing this course and mainly this project.

#### ACKNOWLEDGEMENTS

Foremostly, I would like to thank everyone who had contributed to the successful completion of this project. I would like to express my gratitude and appreciation my supervisor, Amar Faiz Bin Zainal Abidin and the late Ir. Nik Azran Bin Abdul Hadi for their timely advice, guidance and their patience throughout the development of the final year project. The advices and suggestions given are really spot on. Their kind consideration and guidance will always be appreciated. In addition, I would also like to express my gratitude to my loving parent and friends who had helped and given me encouragement throughout the one year duration of this final year project. As for the rest of my friends, who are not named here, rest assured that I am thankful to them as well. Well, what matters the most is the thought, rather than the action.

# **TABLE OF CONTENTS**

		PAGE	
TAB	LE OF CONTENTS	ix	
LIST	<b>FOF TABLES</b>	xiv	
LIST	<b>FOF FIGURES</b>	xvii	
LIST	<b>FOF APPENDICES</b>	xviii	
LIST	<b>F OF SYMBOLS</b>	xix	
LIST	<b>FOF ABBREVIATIONS</b>	xx	
CHA	APTER 1 INTRODUCTION	1	
1.1	Background study	1	
1.2	Problem statement	5	
1.3	Objectives	6	
1.4	1.4Project scopes7		
СНА	APTER 2 LITERATURE REVIEW	8	
2.1	Coupled Tank System	8	
2.2	Operating principles	10	
2.3	Proportional Integral Derivative (PID) as a chosen controller	11	
2.4	What is a PID tuning?	13	
	2.4.1 Basic step for designing a PID controller	13	
	2.4.2 Benefits applying PID controller ix	13	

2	2.5 Sim	ulated Kalman Filter algorithm as a optimization technique	14
	2.5	.1 What is a fitness function in SKF?	15
2	2.6 The	Literature Study on Control Approaches to Coupled Tank System	19
	2.6	1 Genetic Algorithm Tuning Based PID Controller for Liquid-Level	
		Tank System	19
	2.6	2 Double-tank Liquid Level Control Based on Genetic Algorithm	20
	2.6	3 PID Control Tuning Using Cuckoo Search Algorithm for Coupled	
		Tank	21
	2.6	4 Liquid Level Control of a Nonlinear Coupled Tanks System	
		using Fuzzy Logic Control	21
	2.6.	5 Optimal PID Controller for Coupled-Tank Liquid- Level	
		Control System using Bat Algorithm	22
	2.6.	6 Model Predictive Control (MPC) Applied to Coupled Tank	
		Liquid Level System	23
	2.6.7	7 PID Tuning Using Bat Algorithm for Coupled Tank Liquid	
		Level System	24
	2.6.8	3 Optimal PID Controller Parameter for Coupled	
		Tank System Using Priority Fitness Firefly Algorithm	25
	2.6.9	Comparison of LQR and PID Controller Tuning Using	
		PSO for Coupled Tank System	25
	2.6.1	0 Modelling and Control of Coupled Tank Liquid Level	
		System using Backstepping Method	26
	2.6.1	1 PSO-Tuned PID controller for coupled tank system via	
		Priority-base Fitness Scheme	27

	2.6.12 Sliding Mode Control for Coupled-Tank Liquid Level		
		Control System	27
	2.6.13	Performance Comparison between PI and MRAC for	
		Coupled-Tank System	28
	2.6.14	Liquid Level Control of Coupled-Tank System	
		Using Fuzzy-PID Controller	29
	2.6.15	Second Order Sliding Mode Control of MIMO Nonlinear	
		Coupled Tank System	30
	2.6.16	Liquid Level Control of Nonlinear Coupled Tanks System	
		using Linear Model Predictive Control	31
	2.6.17	Active Disturbance Rejection Control of a Coupled-Tank	
		System	32
2.7	Summ	hary	32
СНА	PTER 3	<b>METHODOLOGY</b>	33
3.1	Introd	uction	33
3.2	Research planning and monitoring (K-chart) 34		
3.3	Project methodology 35		
	3.3.1 Flowchart of the project methodology 36		
	3.3.2	Flow chart of the modelling SKF for tuning PID controller of CTS	37
3.4	Propo	sed Mathematical Modelling for Coupled Tank	41
	3.4.1	Basic Nonlinear Model of Coupled Tank System	41
	3.4.2	Model of Linearised Perturbation	43

	3.4.3 Single Input with Single Output (SISO) of Coupled Tank System	
	for First Order Method	45
	3.4.4 Single Input with Single Output (SISO) of Coupled Tank System	
	for Second Order Method	46
3.5	Designing of transfer function for PID Controller	49
3.6	Types of Software Used	51
	3.6.1 MATLAB/Simulink	51
	3.6.2 Simulation of Coupled Tank System	52
СНА	PTER 4 RESULT AND DISCUSSION	55
4.1	Simulation results based PID controller by SKF	55
	4.1.1 3D graph surface for CTS	56
	4.1.2 Best fitness function obtained by SKF	59
	4.1.3 Mode fitness function obtained by SKF	61
	4.1.4 Worst fitness function obtained by SKF	63
4.2	Comparison of simulation results by SKF based main journal	65
СНА	PTER 5 CONCLUSION & FUTURE WORK	66
5.1	Introduction	66
5.2	Conclusion	66
5.3	Future work recommendation	67

## APPENDIX

71

68

## LIST OF TABLES

TABLE	TITLE	PAGE
Table 3.1	Parameter value given of CTS	49
Table 3.2	Calculated parameter value	49
Table 4.1	Parameters value assigned in code development of SKF	56
Table 4.2	Best solution for the best fitness function	59
Table 4.3	Parameters value from graph response of the best fitness	60
Table 4.4	Best solutions for the mode fitness function	61
Table 4.5	Parameter value from graph response of the mode fitness	62
Table 4.6	Best solution for the worst fitness function	63
Table 4.7	Parameters value from graph response of the worst function	64
Table 4.8	Simulation result performance from main journal	65
Table 4.9	Simulation result the performance by SKF optimization	65

# **LIST OF FIGURES**

FIGURE	TITLE	PAGE
Figure 1.1	Coupled tank application in process industry	2
Figure 1.2	Illustration of a typical fluid level structure	3
Figure 2.1	Hardware apparatus of a real coupled tank system	9
Figure 2.2	Schematic diagram	10
Figure 2.3	Proportional integral derivative controller	11
Figure 2.4	The SKF algorithm process flow	18
Figure 2.5	Block diagram of the proposed method for GA technique	19
Figure 2.6	GA-PID control block diagram	20
Figure 2.7	Simulink model for FLC on linear plant model	22
Figure 2.8	The compared response graph	23
Figure 2.9	Simulation model for closed loop MPC	24
Figure 2.10	Schematic diagram for implementation optimization technique	e 26
Figure 2.11	Control structure of CTS with PID controller parameters	27
Figure 2.12	Simulink diagram to simulate MRAC controlled coupled tank	28
Figure 2.13	Simulation of fluid level using PID-Fuzzy	29
Figure 2.14	Schematic of control system process	30
Figure 2.15	Layout of coupled tank	31
Figure 2.16	Block diagram for ARDC for second order system	32

Figure 3.1	K-Chart	34
Figure 3.2	Flow chart of the project methodology	36
Figure 3.3	Flow chart of the modelling SKF for tuning PID controller	40
Figure 3.4	Basic diagram of CTS	41
Figure 3.5	Block diagram of SISO for second order method	48
Figure 3.6	MATLAB/Simulink (R2014a) software	51
Figure 3.7	Overall Simulink diagram of CTS application	52
Figure 3.8	Simulink diagram of transfer function for CTS	53
Figure 3.9	Output water level displayed that set to 10cm as default process	53
Figure 3.10	Block diagram inside the PID controller tune by SKF	54
Figure 4.1	3D graph surface	57
Figure 4.2	Top view of graph pseudocolor from 3D surface	58
Figure 4.3	Convergence curve graph by 50 agents and 450 iterations	59
Figure 4.4	Output graph response of CTS for best fitness function	60
Figure 4.5	Convergence curve graph by 10 agents and 200 iterations	61
Figure 4.6	Output graph response of CTS for mode fitness function	62
Figure 4.7	Convergence curve graph by 10 agents and 150 iterations	63
Figure 4.8	Output graph response of CTS for worst fitness function	62

xvi

# LIST OF APPENDICES

APPENDIX	TITLE	PAGE
Appendix 1	Gantt chart for final year project 1	71
Appendix 2	Gantt chart for final year project 2	72
Appendix 3	Data collected in excel	73
Appendix 4	Convergence curve graph collected	76
Appendix 5	Coding	98

# LIST OF SYMBOLS

α	-	Coefficient discharge
A	-	Cross sectional area
cm	-	Centimeter
d	-	Dimension
e	-	Error
F	-	Fitness
Н	-	Height
K	-	Kalman agent
Р	-	Prior estimate
q	-	Flow rate
Q	-	Process noise
R	-	Measurement noise
S	-	Second
t	-	Time
X	-	State variable
X	-	Estimate state
Xbest	-	Best fitness
Xtrue	-	Best solution so far
Z	-	Linear measurement

## xviii

# LIST OF ABBREVIATIONS

ARDC	Active rejection disturbance controller
CTS	Coupled Tank System
GA	Genetic algorithm
Кр	Proportional gain
Ki	Integral gain
Kd	Derivative gain
MPC	Model predictive controller
MIMO	Multi input multi output
Os	Overshoot
PID	Proportional Integral Derivative
PSO	Particle swarm optimization
PFF	Priority fitness firefly
SMC	Sliding mode controller
SISO	Single input single output
SKF	Simulated Kalman Filter
SSE	Steady state error
Ts	Settling time
Td	Delay time
Тр	Peak time
Tr	Rise time

#### **CHAPTER 1**

#### **INTRODUCTION**

#### 1.1 Background study

In recent years, the performance requirements for chemical, petrochemical and process plants have increased. Development of new production plants to decrease wastage of material, minimize energy consumption, minimize effects on the environment, to cope with ever increasing competition and to satisfy increasing demand for flexibility requires the use of control engineering techniques to provide the desired and efficient control actions with simple and easy control algorithms. Design and implementation of a control system require the use of efficient techniques that provide simple and practical solutions which can fulfil the performance requirements in the face of the disturbances and uncertainties in the process (L. Bissonaise, 2001).

Many researchers over the world interest in the liquid level system application as the technology boom rapidly, in which it typically crucial specifically for an economic increase of the world nowadays. In current years, the performance necessities for chemical, petrochemical and method plants have enlarged. The word "process" in the industries refers to a set of operations to be performed on the different work functions to culminate on any quality assured product. However, in general, the term process tends to be used for both the processing operations and the processing equipment. Figure 1.1 shows all the applications of industries nowadays, which include water treatment facilities, pulp and paper turbines, petrochemical plant and food were as an essential requirement of the liquid level in tanks and fluid drive with the flow within the tanks (S.R. Mahapatro, 2014).



Figure 1.1: Coupled tank application in process industry

The primary objective of the process control is to maintain the process safely and effectively at the desired operating conditions considering the environment and product quality requirements. In association with this, the processing system should respond to transient conditions, such as plant startups and shutdowns, grade changes and unusual disturbances. Without effective process control, it will be difficult, to operate the large scale industrial plants (L. Bissonaise, 2001). Usually, the liquid level in each tank is very commonplace in all procedure manipulate systems today.

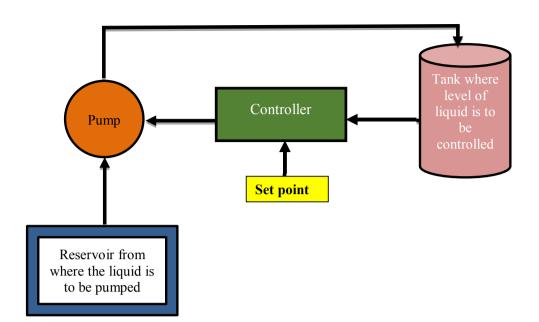


Figure 1.2: Illustration of a typical fluid level structure

Figure 1.2 presents the illustration of a typical fluid level structure commonly in coupled tank system. The coupled tank module as a reservoir which features as storage of water know as a couple tank system. The control of liquid level in tanks and flow between tanks is a basic problem in the process industries. The process industries require liquids to be pumped, stored in tanks, and then pumped to another tank. Many times, the liquids will be processed by chemical or mixing treatment in the tanks, but always the level of fluid in the tanks must be controlled, and the flow between tanks must be regulated. Often the tanks are so coupled together that the levels interact and this must also be controlled (Shahizan, 2008). The level manipulates device must be controlled by the right controller. The goal of the controller in the stage manipulate is to preserve a stage set point at a given value and can receive new set factor values dynamically. The controller will manage the water pump in order to maintain water in each tank in level as required (10cm).

For these significant of the project, the Simulated Kalman Filter (SKF) will be applied to tune the PID parameter controller. Since most of industries are using a PID controller, widely, this project is proposed on using a simple but effective PID controller for the couple's tank system. This is due to simple structure and robust performances in a wide range of operating conditions. (Hazriq et.al., 2015).

By using the PID controller output will obtain in a short time, minimal steady state error and can control the overshoot. The proportional component (Kp) provides an overall control action proportional to the error through the all pass gain factors. The integral component (Ki) was used to minimize steady state error through low frequency compensation. The derivative component used to reduce overshoot and improve transient response through high frequency compensation (Saiful, 2008).

Nevertheless, there are some problems in finding the optimal value of PID parameters. Thus, many researchers have begun to use optimization methods in finding the most appropriate values. Therefore, Simulated Kalman Filter (SKF) is chosen and implemented due to simple optimization compared to the other optimization methods that had been implemented before such as Genetic Algorithm and Cuckoo Algorithm. Developing a simple and effective tuning method for PID controller can significantly contribute to the advancement of control system knowledge and catering the industrial needs.

#### **1.2 Problem statement**

As real-time control involves algorithms to control some certain processes, and used complex algorithm (Shahizan, 2008). In order to study its performance, the control of the level of a coupled tank system is chosen. This application is widely used in the process industry, especially in chemical industries. In this project, controlling liquid level process will be done in real-time by applying Proportional-Integral-Derivative (PID) controller.

A common control problem in process industries is the control of fluids level in storage tanks, chemical blending and reaction vessels (Grega and Maciejczyk, 1994). The flow of liquid into and out of the tank must be regulated as to achieve a constant desired liquid level as fluid to be supplied at a constant rate. Many control algorithms have been implemented using various techniques to compensate with the control requirement. To achieve high performance of the system is by applying state feedback controller to the system.

As the issue of coupled tank liquid level water system demand to be controlled whilst regulating the flow within the tank. In addition, the water level that flow in and flow out from the tanks makes it is very challenging to get a constant of a desired water level. As the parameter of the coupled tank system is simply changed, so the proper optimization tuning method will be approachable to beat this issue.

5